Amendments to the Specification:

Please replace the paragraph beginning on page 1, line 12 with the following rewritten paragraph:

-- Deposition technologies are typically defined as technologies that deposit functional materials dissolved and/or dispersed in a fluid onto a receiver (also commonly known as substrate etc.). Technologies that use supercritical fluid solvents to create thin films are known. For example, R. D. Smith in U.S. Pat. No. 4,582,731, U.S. Pat. No. 4,734,227 and U.S. Pat. No. ~~4,743,451~~ 4,734,451 discloses a method involving dissolution of a solid material into a supercritical fluid solution and then rapidly expanding the solution through a short orifice into a region of relatively low pressure to produce a molecular spray. This may be directed against a substrate to deposit a solid thin film thereon, or discharged into a collection chamber to collect a fine powder. By choosing appropriate geometry of the orifice, and maintenance of temperature, the method also allows making of ultra-thin fibers from polymers. This method is known as RESS (rapid expansion of supercritical solutions) in the art.--

Please replace the paragraph beginning on page 8, line 5 with the following rewritten paragraph:

-- FIGS. ~~4A~~ 4C-4K are cross sectional views of a portion of the system shown in FIG. 1A.--

Please replace the paragraph beginning on page 12, line 8 with the following rewritten paragraph:

-- In accordance with a preferred embodiment of the invention, the solvent/desired substance solution and compressed fluid antisolvent are contacted in a particle formation vessel by introducing feed streams of such components into a highly agitated zone of the particle formation vessel, such that the first solvent/solute feed stream is dispersed in the compressed fluid by action of a rotary agitator as described in concurrently filed, copending, commonly assigned USSN 10/814,354 ~~(Kodak Docket No. 86430)~~, the disclosure of which is incorporated by reference herein. As described in such copending application, effective micro and meso mixing, and resulting intimate contact of the feed stream components, enabled by the introduction of the feed streams into the

vessel within a distance of one impeller diameter from the surface of the impeller of the rotary agitator, enable precipitations of particles of the desired substance in the particle formation vessel with a volume-weighted average diameter of less than 100 nanometers, preferably less than 50 nanometers, and most preferably less than 10 nanometers. In addition, a narrow size-frequency distribution for the particles may be obtained. The measure of the volume-weighted size-frequency distribution, or coefficient of variation (mean diameter of the distribution divided by the standard deviation of the distribution), e.g., is typically 50% or less, with coefficients of variation of even less than 20% being enabled. The size-frequency distribution may therefore be monodisperse. Process conditions may be controlled in the particle formation vessel, and changed when desired, to vary particle size as desired. Preferred mixing apparatus which may be used in accordance with such embodiment includes rotary agitators of the type which have been previously disclosed for use in the photographic silver halide emulsion art for precipitating silver halide particles by reaction of simultaneously introduced silver and halide salt solution feed streams. Such rotary agitators may include, e.g., turbines, marine propellers, discs, and other mixing impellers known in the art (see, e.g., U.S. 3,415,650; U.S. 6,513,965, U.S. 6,422,736; U.S. 5,690,428, U.S. 5,334,359, U.S. 4,289,733; U.S. 5,096,690; U.S. 4,666,669, EP 1156875, WO-0160511).--